

CHAPTER 4

SIMULTANEOUS DEPOSITION OF ALLOYS



• Electro deposition of Alloys :

4.1 Introduction :

Although metals are highly valued in the pure state, they are usually not strong enough to satisfy the present exacting demands of structural and mechanical engineering. However if the metals are judiciously alloyed, we get materials with requisite properties to withstand the stresses and strains of the present day needs. Also, codeposition of metals results in an appreciable reduction in metal cost. Furthermore, alloys can be used for decorative purposes, in view of their special and variable colour effects.

The problems arising in the deposition of alloys are the composition of the solution, the choice of electrodes (anodes in particular) and the conditions of operation in order to secure the required composition in the deposited alloy. The chemical equivalent of the two constituents influences their proportion in the deposit, as the solution will not necessarily contain the alloy constituents in the same proportion as that of the required alloy deposit. Further anode and cathode efficiencies are not likely to balance and this leads to variation in the composition of the solution. To avoid this insoluble anodes are used wherever possible.

4.2 Co-deposition of metals : Simultaneous Discharge of Cations:

If a solution contains two cations, there is a possibility that simultaneous discharge may occur. This problem is very

interesting in the electrodeposition of alloy. But this problem is also very important in the deposition of single metals, since the aqueous solutions always contain hydrogen ions. Were it not for a variety of complicating factors, such as the influence of one metal on the deposition potential of the other, the situation would in principle be relatively simple. Provided the discharge potentials of the two ions were the same, simultaneous deposition would occur.

For example the reversible potential of a metal A in a solution of its ions of activity a_A + I.e. of the electrode A, E would be given by

$$E = E_A^0 - \frac{RT}{4F} \ln a_A^{+} \quad \dots (1)$$

and the theoretical discharge potential E_{dis} is equal to $-E$ I.e.

$$E_{dis} = -E_A^0 + \frac{RT}{4F} \ln a_A^{+} \quad \dots (2)$$

In order to obtain the actual discharge potential, it is necessary to include the over voltage η_A , and so it follows that

$$E_{dis} = -E_A^0 - \eta_A + \frac{RT}{4F} \ln a_A^{+} \dots (3)$$

If the solution contains two cations, one of which may be the hydrogen ion, ~~is~~ provided there is no interaction in solution or in the deposit, simultaneous deposition will occur when the two discharge potentials, e.g. of A and H,

become equal, that is, when

$$-\frac{E_h^0 - E_b}{\frac{RT}{F}} \ln a_1 + n = -\frac{E_b^0 - E_b}{\frac{RT}{F}} \ln a_2 + .. \quad (4)$$

The subject of simultaneous discharge may be divided into two aspects, first, when it is desired to deposit two metals simultaneously, e.g. in alloy deposition, and second, when simultaneous deposition is to be avoided, e.g. in electro-analytical work. We are concerned with the former.

An examination of equation (4) shows that there are in general, three ways in which the discharge potentials of two cations may be brought together : (i) if the standard potentials are different, but the overvoltages very sufficiently to compensate for this difference, and (ii) if the differences in reversible potentials and overvoltages are compensated for by differences in activities (concentrations) of the ions. (iii) if E° of the two are equal and overvoltages are small.

4.3 Influence of Plating Parameters in Alloy Deposition :

Independent parameters in alloy deposition, as in all deposition, processes are current density, temperature, agitation, pH and concentrations of bath constituents. Normally, these must be more tightly controlled in alloy plating than in single metal plating, because it is likely that a change in any one will affect one metal more than the other and thus changes the composition of the alloy. Exact effects can be determined only by experiment. Current efficiency, addition agents, basic metal, stirring power and anode have a profound

role in alloy deposition (71,72).

Many alloy deposition baths (viz., simple and complex, organic solvent baths) are possible, so that failure with one type in no way proves that the deposition of a given alloy is impractical (73).

4.4. Electrodeposition of Nickel-Chromium Alloys

The Aim and Scope of the Present Work ^ Earlier Work:

The studies under consideration deal with the electrodeposition of nickel-chromium alloys. It is of interest to note that most of the work done in the past, is largely of qualitative nature and quantitative information available on the subject is very little. The number of combinations of the platable metals in the form of alloys is very large. The alloy deposits, obtained electrolytically are not always sound, coherent, thick, lustrous and smooth so that they can have any practical value. Very few alloy systems have made their way from laboratory to plant and fewer still have evolved into fairly wide spread practical applications. However, there are immense possibilities of novel nature in the studies, if seriously thought from technological as well as theoretical stand point. Cast and wrought nickel-chromium alloys give excellent wear resistance, corrosion resistance, electrical resistance, and high hot strength. Electrodeposited alloy coatings probably have similar properties and would allow a cheap substrate to be used, thus eliminating the need for more expensive cast or

wrought alloys. Hence numerous attempts have been made to develop a suitable commercial plating process. Reviews by Arrowsmith (1) and Zimblin (73) indicate that no such process has yet been produced. However good quality deposits were reported from a bath containing potassium chromate sulphate, nickel formate, tetrachloro chloroform, boric acid, sodium fluoride, and glycine (75). The current efficiency of the process is not high. A patent on a bath containing dipolar organic compound claims that chromium plated coatings can be electrodeposited over a wide range of current densities with adequate current efficiencies (1-2). Studies on the outdoor corrosion resistance (76) and the behaviour of Ni-Cr electrodeposits in industrial, marine and urban environments indicate the value of such plates when used for decorative purposes (7,78). Attempts have also been made to obtain an alloy deposit of Ni-Cr-Fe, having an appearance and properties of stainless steel (79).

The aim of the present work is to make an attempt for systematic, exhaustive and quantitative study on electrodeposition of binary alloy of nickel and chromium and to establish optimum conditions to obtain the best quality deposit. The influence of the following parameters is studied in greater details to establish the optimum conditions under each system.

- 1) Composition of the Bath (Electrolyte concentrations),
- 2) Temperature,
- 3) Current Density,
- 4) Curation of Electrolyte,

5) Electrode Distance.

6) Addition Agents.

With the help of certain addition agents, we have succeeded in obtaining an alloy deposit of high quality and properties which may bring about a radical change in the plating industry. Considering increasing cost of noble metals, inclusion of silver or gold in traces in the solution has evolved a new method of obtaining an alloy deposit with hitherto unknown properties.

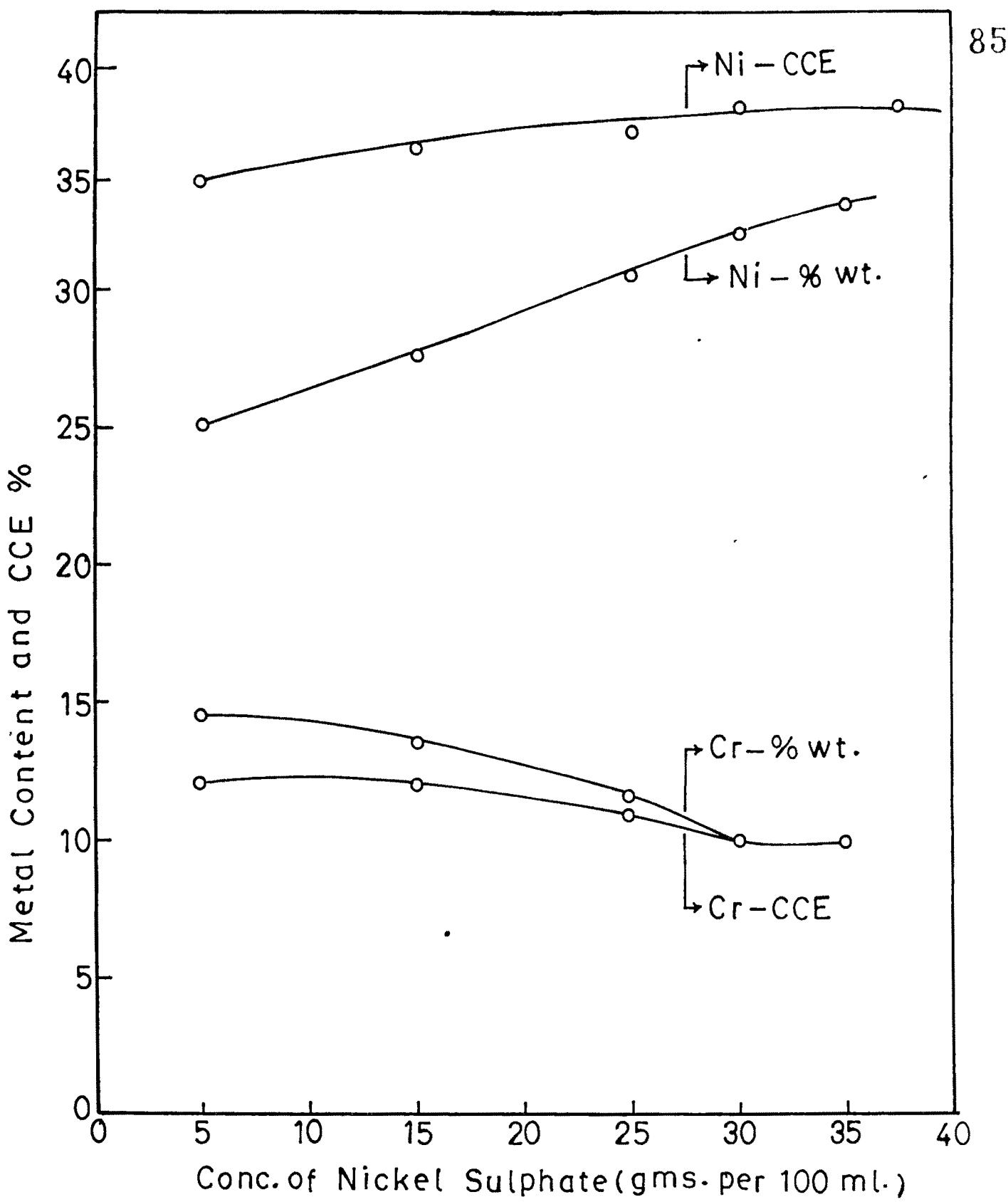


Fig. 17—Effect of conc. of Nickel Sulphate on CCE % of the Nickel Chromium alloy deposit.



TABLE 30-282- The effect of concentration of potassium chloride current efficiency (C.E.) of nickel-chromium alloy deposit.

Nickel sulphate : 25 gms. per 100 ml. Potassium thiocyanate : 5 gms. per 100 ml.
 Currents : 4 A.C. per 100 ml. Current density : 2.4 ampes. per sq. dm.
 Temperature : 25°C. Duration of electrolysis : 20 minutes.
 Electrode distance : 4 cm.
 Voltage : 2.0 to 3 volt(s).

| Obs. | Conc. of KCl, gm. | Per cent deposit on anodic substrate | Metal content in alloy deposit, % as deposit | Effect | | | Nature of deposit. |
|------|----------------------|---|--|--------|-------|-------|--|
| | | | | C.E. | S.E. | C.E. | |
| 1 | 5 | 0.174 | 0.050 | 70.00 | 24.00 | 26.03 | 36.19 dark black nonadherent. |
| | | 0.146 | 0.050 | 70.58 | 25.69 | 26.46 | 19.79 37.25 dark black at edges. |
| 2 | 10 | 0.086 | 0.034 | 73.53 | 26.47 | 31.20 | 12.70 43.90 slight improvement. |
| | | 0.084 | 0.033 | 72.73 | 27.27 | 30.56 | 12.98 43.64 |
| 3 | 15 | 0.125 | 0.044 | 65.91 | 21.31 | 24.30 | 13.57 38.47 dull white, adherent, |
| | | 0.125 | 0.045 | 64.44 | 31.11 | 24.90 | 13.57 38.47 |
| 4 | * 20 | 0.135 | 0.046 | 63.04 | 31.11 | 24.86 | 13.57 38.43 white with slight black shade, adherent. |
| | | 0.125 | 0.047 | 62.83 | 31.11 | 25.76 | 13.57 36.42 |
| 5 | 25 | 0.125 | 0.046 | 63.04 | 31.11 | 24.96 | 13.57 36.49 black slightly nonadherent. |
| | | 0.125 | 0.045 | 63.04 | 31.11 | 24.86 | 13.57 36.42 |
| 6 | 35 | - | - | - | - | - | - |

* Optimum condition.

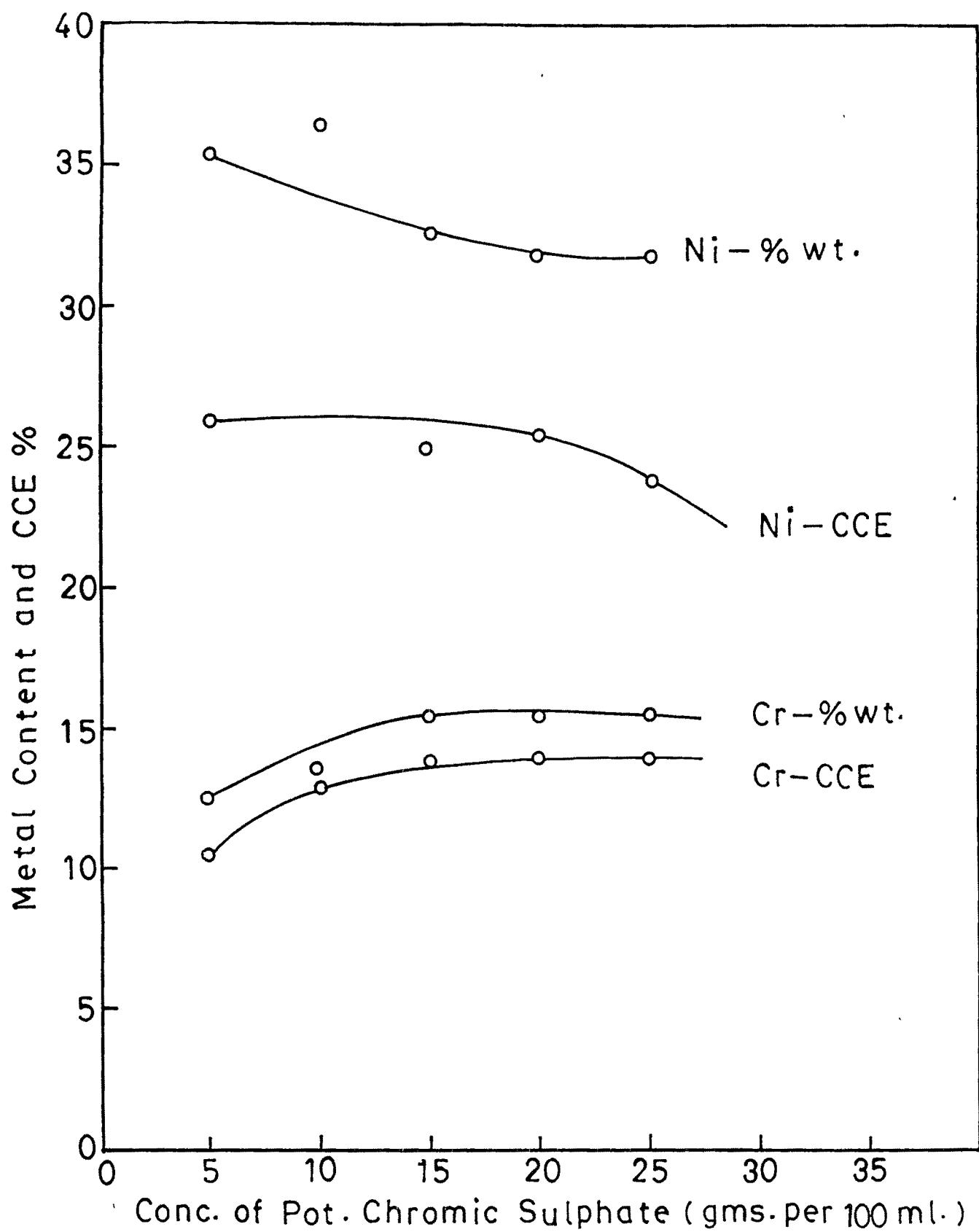


Fig. 18 — Effect of conc. of Potassium Chromic Sulphate
on the metal content and CCE % of the
Nickel Chromium alloy deposit.

TABLE 10.19 2- THE EFFECT OF CONCENTRATION OF POTASSIUM CHLOROPLATE ON THE METAL CONTENT AND THE PERCENTAGE CATHODE CURRENT EFFICIENCY (3.3% H₂O) OF NICKEL-COPPER ALLOY DEPOSIT.

Nickel sulphate : 25 gms. per 100 ml.
Glycine : 6 gms. per 100 ml.
Temperature : 25°C.
Concentration of electrolyte : 20 mmoles.
Anode : 0.032 mm².
Copper deposited per 100 ml. in coulombs : 112.0
Current density : 2.4 amp./per sq.cm.
Electrode distance : 4 cms.
Voltage : 2.9 volts.

| Obs. No. | Conc. of pot. thio-cyanate in gms. | Cath. current in gms. | Wt. of metal content in deposit % | Cath. % | | Total Cath. % | Nature of deposit. |
|----------|------------------------------------|-----------------------|-----------------------------------|---------|-------|---------------|------------------------------------|
| | | | | Cu | Ni | | |
| 1 | 2 | 0.110 | 0.032 | 52.50 | 37.50 | 19.51 | 13.22 32.73 Slight nonuniformity. |
| | | 0.110 | 0.032 | 53.63 | 34.38 | 19.94 | 13.90 33.34 dull & white. |
| 2 | 4 | 0.110 | 0.034 | 59.82 | 36.23 | 19.19 | 13.35 31.56 slight improvement |
| | | 0.110 | 0.035 | 60.90 | 40.90 | 18.96 | 14.25 33.19 |
| 3 | 6 | 0.120 | 0.057 | 56.76 | 35.16 | 18.78 | 13.13 31.91 Adherence, dull white. |
| | | 0.119 | 0.036 | 58.33 | 33.33 | 18.94 | 12.23 31.17 |
| 4 | 8 | 0.120 | 0.060 | 57.50 | 35.0 | 19.28 | 13.25 32.53 |
| | | 0.127 | 0.040 | 57.50 | 35.0 | 19.44 | 13.36 32.80 |
| 5 | 10 | 0.135 | 0.071 | 58.54 | 34.15 | 19.05 | 12.56 31.64 |
| | | 0.135 | 0.040 | 60.00 | 35.00 | 19.08 | 12.56 31.64 |
| | | | | | | | -30- |

* Optimum condition.

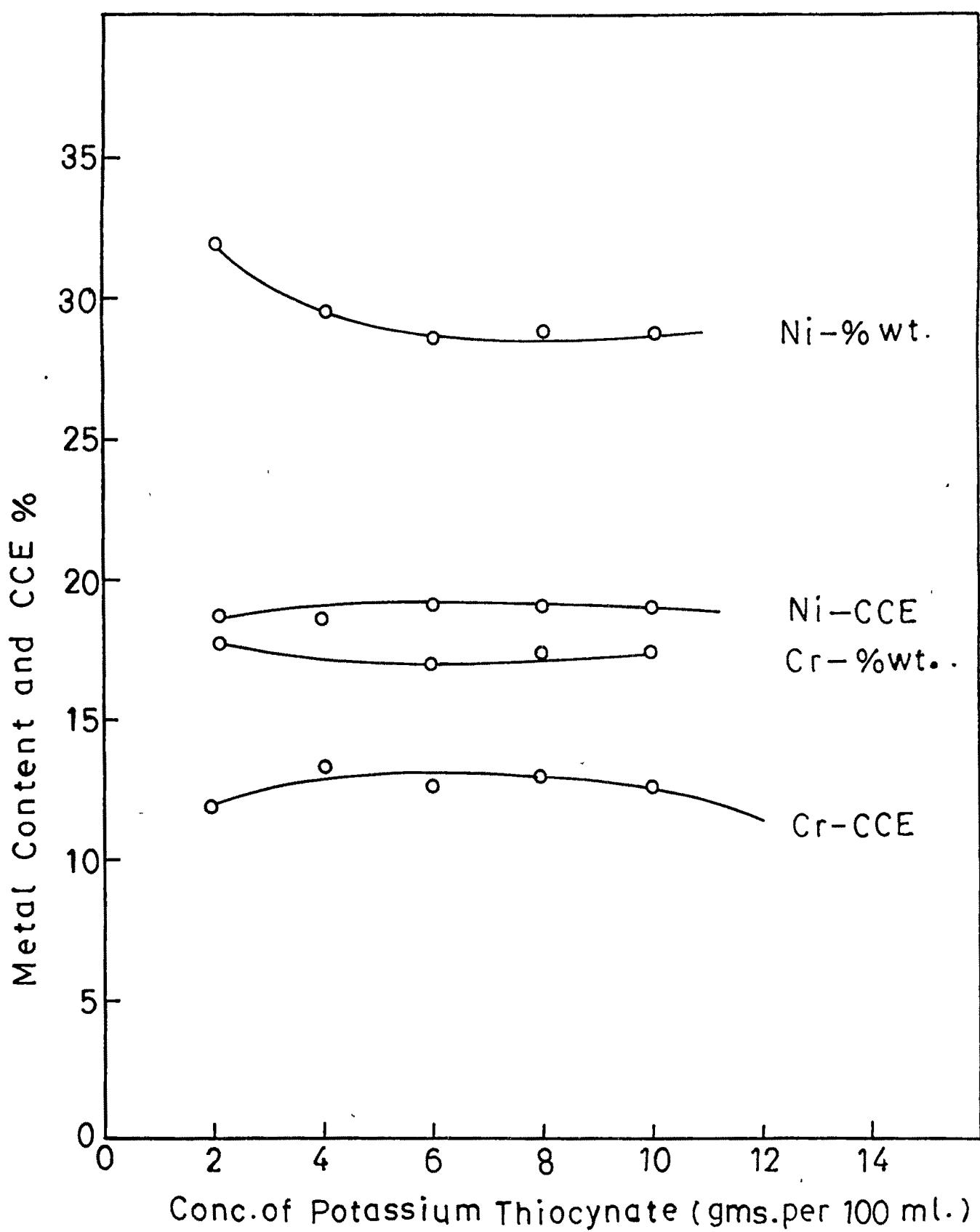


Fig. 19 – Effect of conc. of Potassium Thiocyanate on the metal content and CCE % of the Nickel – Chromium alloy deposit.

TABLE NO. 20 :- The effect of concentration of glycine on the metal content and the percentage cathode current efficiency (CEE %) of Nickel-chromium alloy deposit.

Nickel sulphate : 25 gms. per 100 ml.
Potassium chromate : 2.4 gms. per 50 ml.
Current density : 2.4 ampes. per 50 cm.
Duration of electrolysis : 30 minutes
Temperature : 25°C.
Anode distance : 4 cms.

| Obs. | Conc. of glycine per 100 ml. gm. | Per cent deposit in chro- mated water. | Metal content in deposit in gm. | CEE % | | | Nature of deposit | | |
|------|--|--|---------------------------------------|-------|-------|-------|-------------------|-------|--------------------------|
| | | | | Cat. | Cr. | Cl. | | | |
| 1 | 0 | 0.110 | 0.030 | 60.00 | 33.33 | 17.56 | 12.12 | 29.68 | Nonsolvent, black |
| | 0.111 | 0.030 | 60.00 | 33.33 | 17.40 | 12.01 | 12.01 | 39.41 | |
| 2 | + 2 | 0.115 | 0.033 | 57.50 | 39.40 | 17.73 | 13.70 | 31.43 | Adherent, black |
| | 0.114 | 0.033 | 57.50 | 39.40 | 17.89 | 13.91 | 13.70 | | |
| 3 | * 4 | 0.120 | 0.030 | 57.89 | 39.47 | 16.92 | 15.14 | 36.06 | Adherent, blackish-white |
| | 0.120 | 0.030 | 57.89 | 39.47 | 16.92 | 15.14 | 15.14 | 36.06 | |
| 4 | 6 | 0.122 | 0.030 | 57.50 | 37.50 | 20.23 | 16.51 | 34.77 | Black, adherent |
| | 0.123 | 0.040 | 57.50 | 40.00 | 19.75 | 15.51 | 15.51 | 35.26 | |
| 5 | 8 | 0.123 | 0.042 | 59.52 | 40.40 | 21.81 | 16.74 | 39.55 | - - - - - |
| | 0.123 | 0.041 | 59.54 | 41.46 | 20.94 | 16.74 | 16.74 | 37.68 | |

* Optimum condition. + cf. Plate 11.

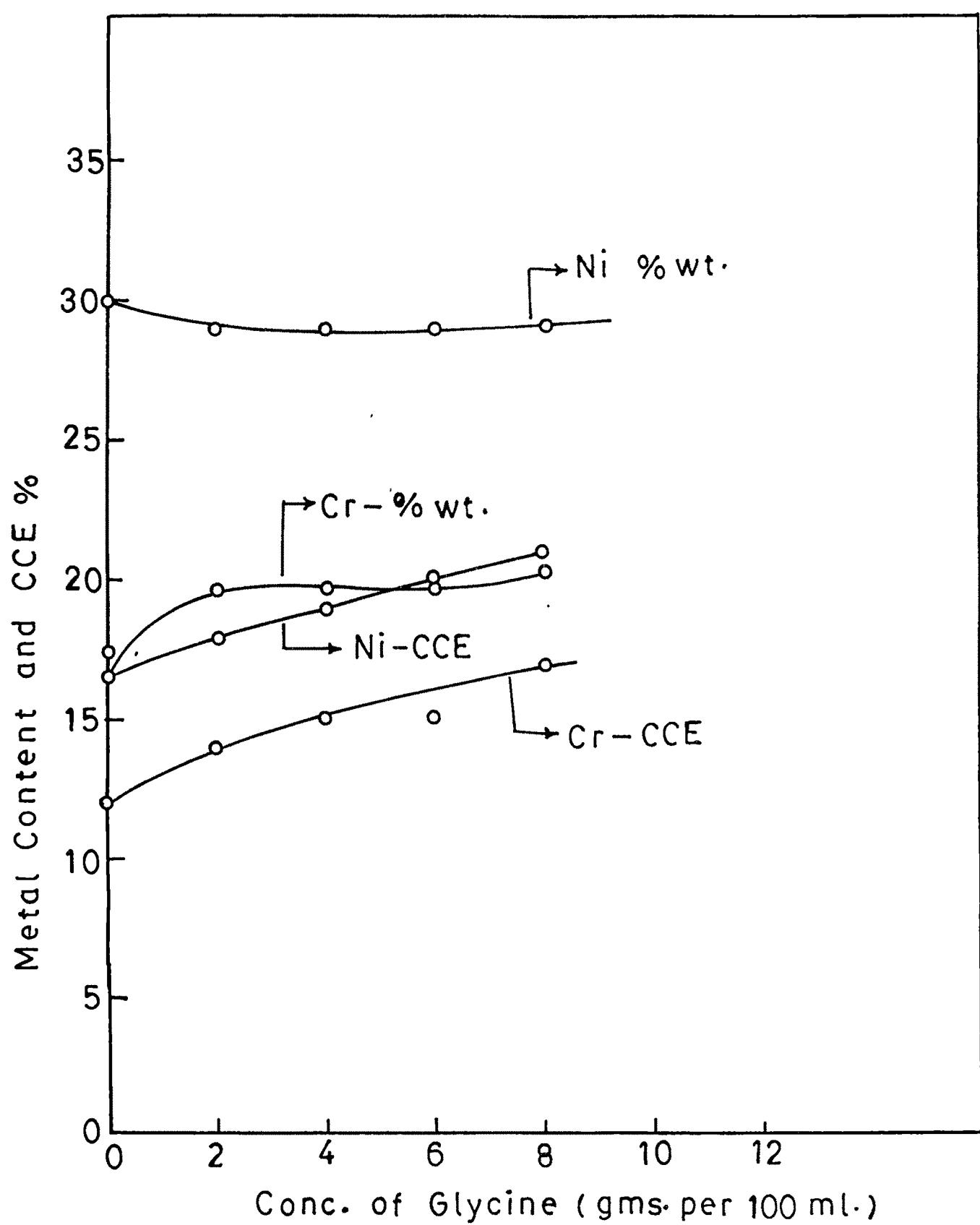


Fig. 20—Effect of conc. of Glycine on the metal content and CCE % of the Nickel Chromium alloy deposit.

TABLE 102,21. - The effect of current density on the metal content and the percentage of deposit.

Machal sulfite : 25 gms. per 100 ml. Potassium chloride sulphate : 10 gms. per 100 ml.
 Potassium chloride : 5 gms. per 100 ml. Glycine : 6 gms. per 100 ml.
 Temperature : 25° Celsius ± 20 minutes.
 Electrode distance : 3 cm.
 Voltage : 2.4 to 3.00 volts.

| Obs. | Current no. | Ct. of deposit alloy deposit | Ct. of metal content in deposit alloy | | Total Ct. | Nature of deposit. |
|------|----------------|------------------------------------|--|-----------|--------------|--------------------|
| | | | Per cent. | Per cent. | | |
| 1 | 0.8 | 0.030 | 0.020 | 75.00 | 20.14 | 6.06 |
| | 0.030 | 0.020 | 0.020 | 75.00 | 20.05 | 6.05 |
| 2 | 1.6 | 0.120 | 0.035 | 71.42 | 25.71 | 22.33 |
| | 0.121 | 0.035 | 0.035 | 72.32 | 20.37 | 22.17 |
| 3 | * 2.4 | 0.143 | 0.052 | 71.13 | 25.32 | 26.03 |
| | 0.143 | 0.032 | 0.032 | 71.15 | 26.22 | 26.03 |
| 4 | + 3.2 | 0.160 | 0.060 | 71.01 | 24.63 | 21.33 |
| | 0.166 | 0.065 | 0.065 | 73.63 | 26.15 | 21.30 |
| 5 | 4.0 | 0.210 | 0.037 | 74.71 | 23.23 | 23.22 |
| | 0.202 | 0.037 | 0.037 | 74.71 | 25.20 | 23.23 |

* Optimum conditions. + cf. Plate 12

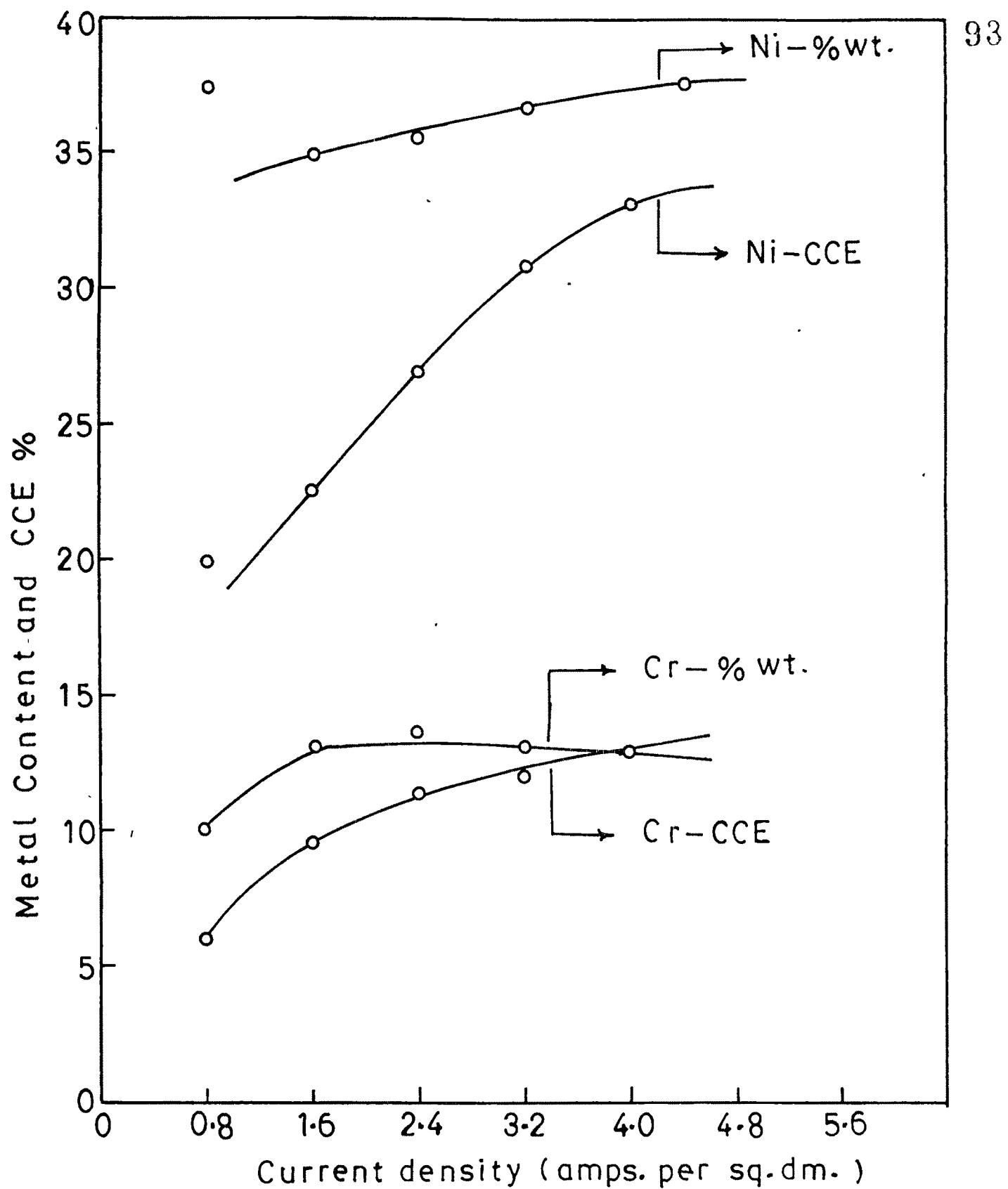


Fig. 21 – Effect of current density on the metal content and CCE % of the Nickel Chromium alloy deposit .

TABLE NO. 22 - The effect of temperature on the metal content and the percentage carbide.

Block graphite : 25 cps.-per 100 ml. potassium chromate substrate : 20 cps.-per 100 ml.
 Potassium chromate : 16 gms.-per 100 ml. Zincine : 4 cps.-per 100 ml.
 Current density : 2.4 amps.-per 50-60. Duration of electrolysis : 20 minutes
 Electrode distance : 4 cmns. Voltage : 2 to 2.3 volts.

| No. | Tempere- ature ° C. | % of metal content | | COP % | | Total nitride of copper | | |
|-----|---------------------------|-------------------------|------------------------|-------|-------|----------------------------|-------|-------|
| | | in copper deposit | in copper matrix | Cu | Fe | Cu | Fe | |
| 1 | 15 | 0.130 | 0.035 | 62.35 | 34.29 | 19.16 | 29.34 | |
| | 0.131 | 0.037 | 59.46 | 37.84 | 18.02 | 12.95 | 38.37 | |
| 2 | 25 | 0.145 | 0.042 | 60.29 | 35.71 | 19.98 | 11.10 | 31.08 |
| | 0.146 | 0.039 | 55.26 | 39.47 | 17.63 | 12.98 | 30.61 | |
| 3 | + 35 | 0.163 | 0.050 | 66.00 | 30.00 | 23.13 | 12.87 | 37.01 |
| | 0.163 | 0.032 | 59.62 | 36.53 | 20.40 | 14.12 | 37.02 | |
| 4 | 45 | 0.146 | 0.040 | 62.50 | 37.50 | 18.38 | 12.85 | 30.88 |
| | 0.143 | 0.040 | 62.50 | 37.50 | 18.38 | 12.45 | 30.83 | |
| 5 | 55 | 0.145 | 0.041 | 63.41 | 34.15 | 18.34 | 11.78 | 30.98 |
| | 0.141 | 0.039 | 61.54 | 41.03 | 18.27 | 13.75 | 32.02 | |

* Optimum condition. + Cf. Plate 13

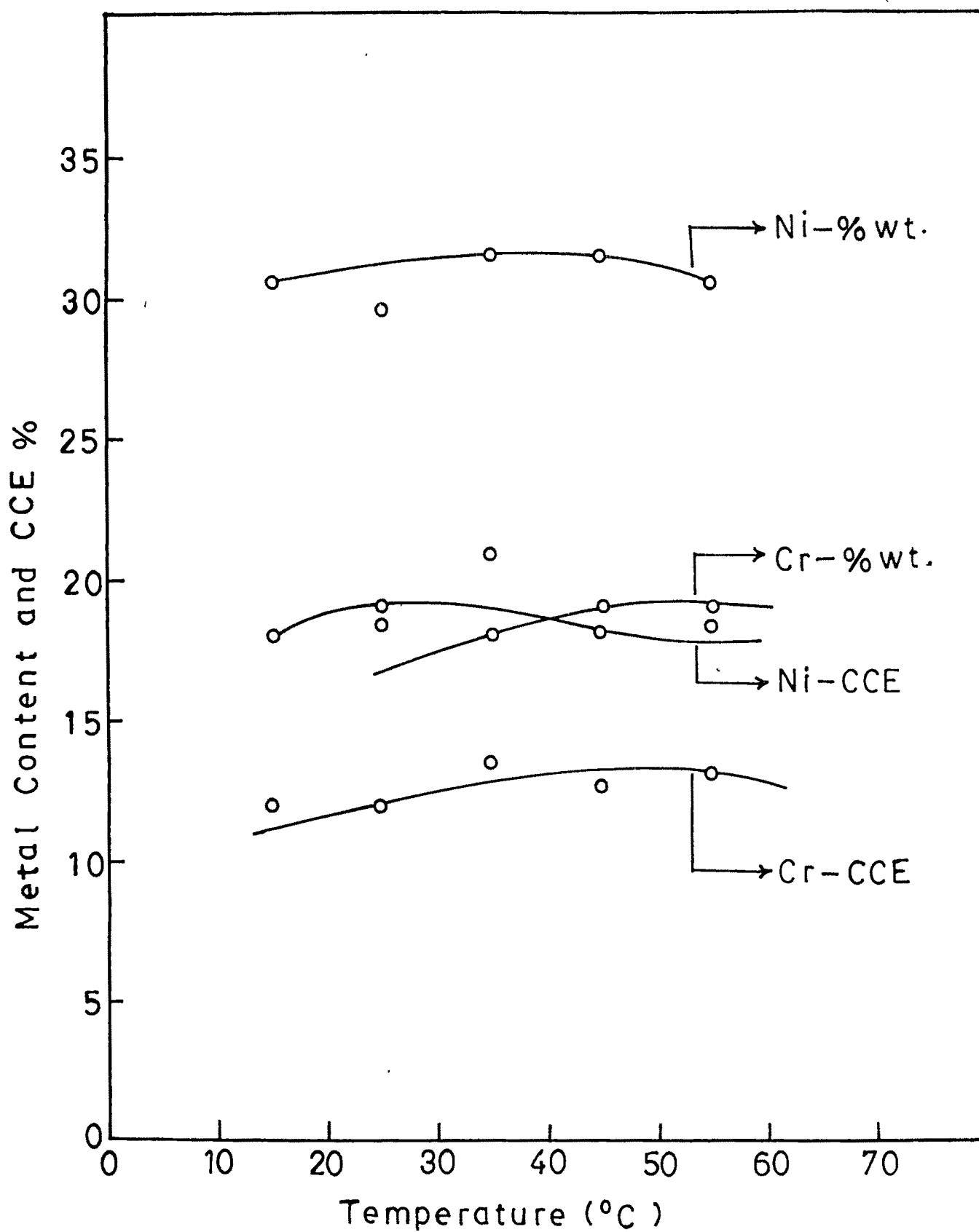


Fig. 22—Effect of temperature on the metal content and CCE % of the Nickel Chromium alloy deposit.

TABLE III*^a - The effect of duration of electrolysis on the metal content and the percentage removal of current efficiency (in %) of nickel-chloride alloy deposit.

Nickel sulphate : 25 gms. per 100 ml. Potassium chloride : 10 gms. per 100 ml.
 Potassium thiocyanate : 5 gms. per 100 ml. Glycine : 4 gms. per 100 ml.
 Current density : 2 A/cm². per 30°.S.H. Temperature : 35°C.
 Electrode distance : 6 cm.^b Voltage : 2 V.D.C.

| Time of electrolysis minutes | Current density A/cm ² | Effect of current on metal content | | | Total current efficiency % | Nature of deposit |
|---------------------------------|--------------------------------------|---------------------------------------|-------|-------|-------------------------------------|-----------------------|
| | | 1 hr. | 2 hr. | 3 hr. | | |
| 1 | 0.055 | 62.50 | 31.25 | 19.51 | 11.01 | 90.52 |
| 2 | 0.055 | 64.40 | 20.41 | 21.00 | 10.81 | 31.89 |
| 3 | 0.055 | 68.53 | 33.33 | 21.45 | 12.75 | 34.21 |
| 4 | 0.055 | 64.52 | 35.48 | 22.36 | 12.58 | 35.26 |
| 5 | 0.150 | 72.00 | 36.00 | 24.30 | 13.71 | 39.01 |
| 6 | 0.160 | 69.42 | 36.54 | 26.15 | 14.38 | 38.53 |
| 7 | 0.175 | 64.00 | 33.00 | 25.76 | 14.53 | 40.06 |
| 8 | 0.200 | 65.28 | 32.00 | 25.20 | 14.31 | 40.42 |
| 9 | 30 | - | - | - | - | Mulli white adherent. |

* Optimum condition. -f. Table I4.

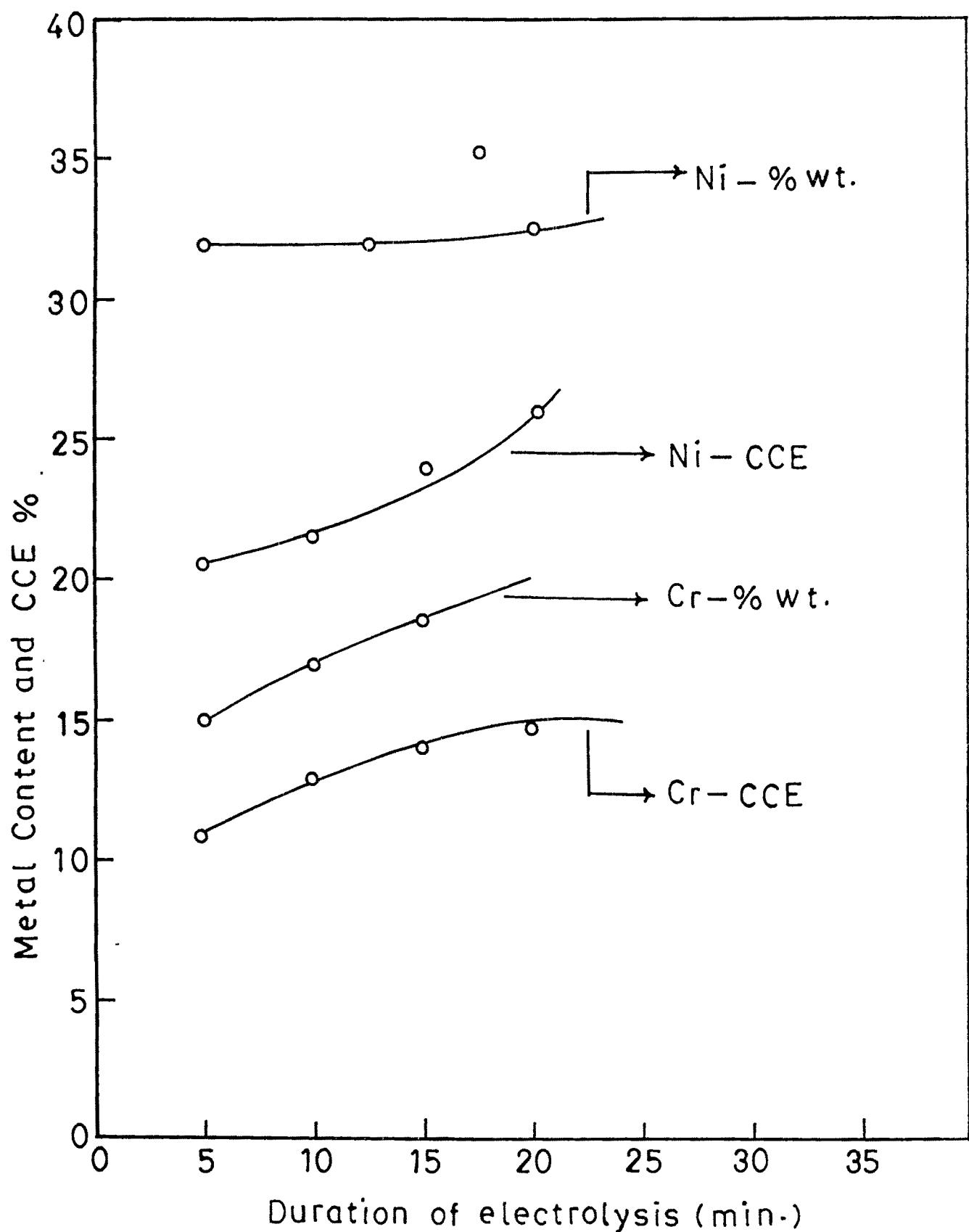


Fig.23—Effect of duration of electrolysis on the metal content and CCE % of the Nickel Chromium alloy deposit.



TABLE NO. 24 - The effect of electrode distance on the total current efficiency (%) ofnickel-chromium alloy deposits.

Nickel sulphate : 25 gms. per 100 ml.
potassium chromate : 6 gms. per 100 ml.
Glycine : 4 gms. per 100 ml.
Chromium : 2.4 gms. per 100 ml.
Temperature : 35°C
Voltage : 2 to 2.5 volts.
Duration of electrolysis : 20 minutes.

| No. | Electrode set-up No. of copper electrodes demolished in collector meter | Current gms. | Metal content in alloy deposit | | Total % G.E. | Nature of deposit G.E. | Nature of deposit G.E. |
|-----|---|-----------------|-----------------------------------|-------|-----------------|---------------------------|---------------------------|
| | | | Cr. | Ni. | | | |
| 1 | 1 | 0.130 | 0.037 | 50.66 | 37.86 | 18.82 | 13.06 |
| | | 0.130 | 0.037 | 50.45 | 37.84 | 18.52 | 13.06 |
| 2 | 2 | 0.132 | 0.039 | 50.97 | 31.32 | 10.70 | 11.93 |
| | | 0.130 | 0.039 | 55.26 | 34.81 | 27.34 | 13.71 |
| 3 | 3 | 0.129 | 0.036 | 61.21 | 30.45 | 10.30 | 10.33 |
| | | 0.130 | 0.036 | 55.58 | 35.36 | 20.26 | 10.33 |
| 4 | 4 | 0.130 | 0.036 | 58.98 | 37.70 | 17.38 | 9.32 |
| | | 0.132 | 0.036 | 55.34 | 37.78 | 17.20 | 9.25 |
| 5 | 5 | - | - | - | - | - | - |

White deposit with
some black patches.

* Optimum condition. Cf. Plate 14.

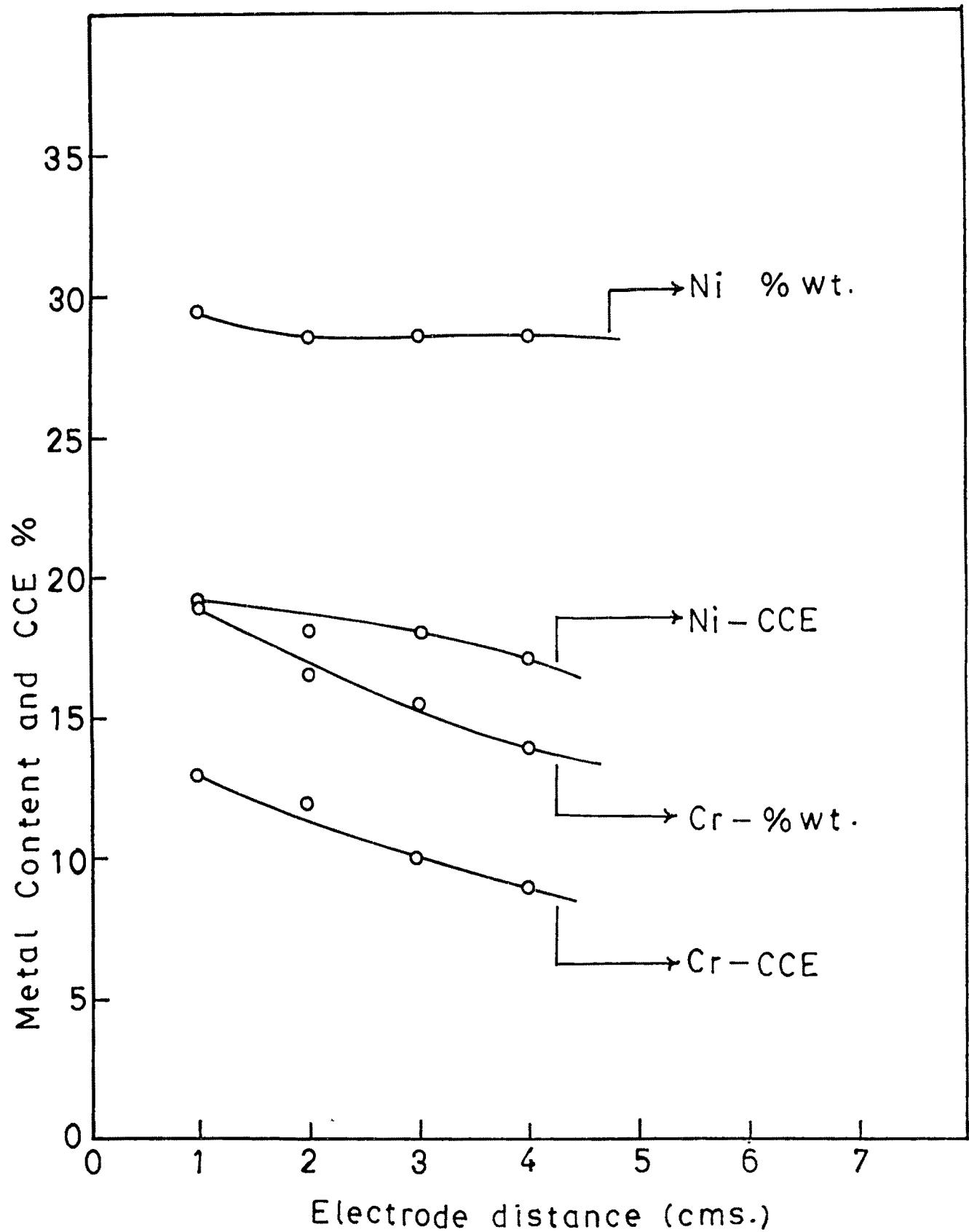


Fig. 24—Effect of electrode distance on the metal content and CCE % of the Nickel Chromium alloy deposit.

TABLE NO. 25 :- The effect of addition agents on the metal content and the percentage adherence current efficiency (%) of the nickel - carbonyl alloy deposit.

Nickel sulphate : 25 gms. per 100 ml. Potassium carbonate : 4 gms. per 100 ml. Potassium thioacetate : 6 gms. per 100 ml. Glycerine : 4 gms. per 100 ml. Current density : 2.4 amp. per sq. dm. Duration of electrolysis : 26 minutes. Electrode distance : 2 cms. Voltage : 2 to 2.3 volts.

| Obs. No. | Addition agent | Current in amp. per 100 ml. | It. of deposit deposited in coulombs per meter | Metal content in alloy deposit | | | CBS % | Nature of deposit |
|----------|------------------|-----------------------------|--|--------------------------------|-------|-------|-------|---------------------------------------|
| | | | | Ges. | U.P. | C.R. | | |
| 1 | Urea | 0.3 gms. | 0.125 | 0.034 | 61.76 | 32.35 | 29.03 | 10.66 20.69 No improvement in quality |
| 2 | Chitosan | - | 0.125 | 0.034 | 58.92 | 35.29 | 17.03 | 11.54 23.57 |
| 3 | Open | - | 0.125 | 0.036 | 60.53 | 36.04 | 19.75 | 13.57 33.32 Brightness enhanced |
| 4 | Nicotinase | - | 0.125 | 0.037 | 60.53 | 35.14 | 19.75 | 12.60 32.35 |
| 5 | Sorbit | - | 0.140 | 0.040 | 72.50 | 25.00 | 22.23 | 8.65 30.83 Bright white adherent |
| 6 | * Silver nitrate | - | 0.130 | 0.034 | 67.64 | 26.42 | 18.99 | 8.39 27.38 Smooth, bright |
| 7 | Sulphuric acid | - | 0.128 | 0.033 | 66.67 | 33.30 | 18.44 | 9.45 27.93 slight nonadherent |

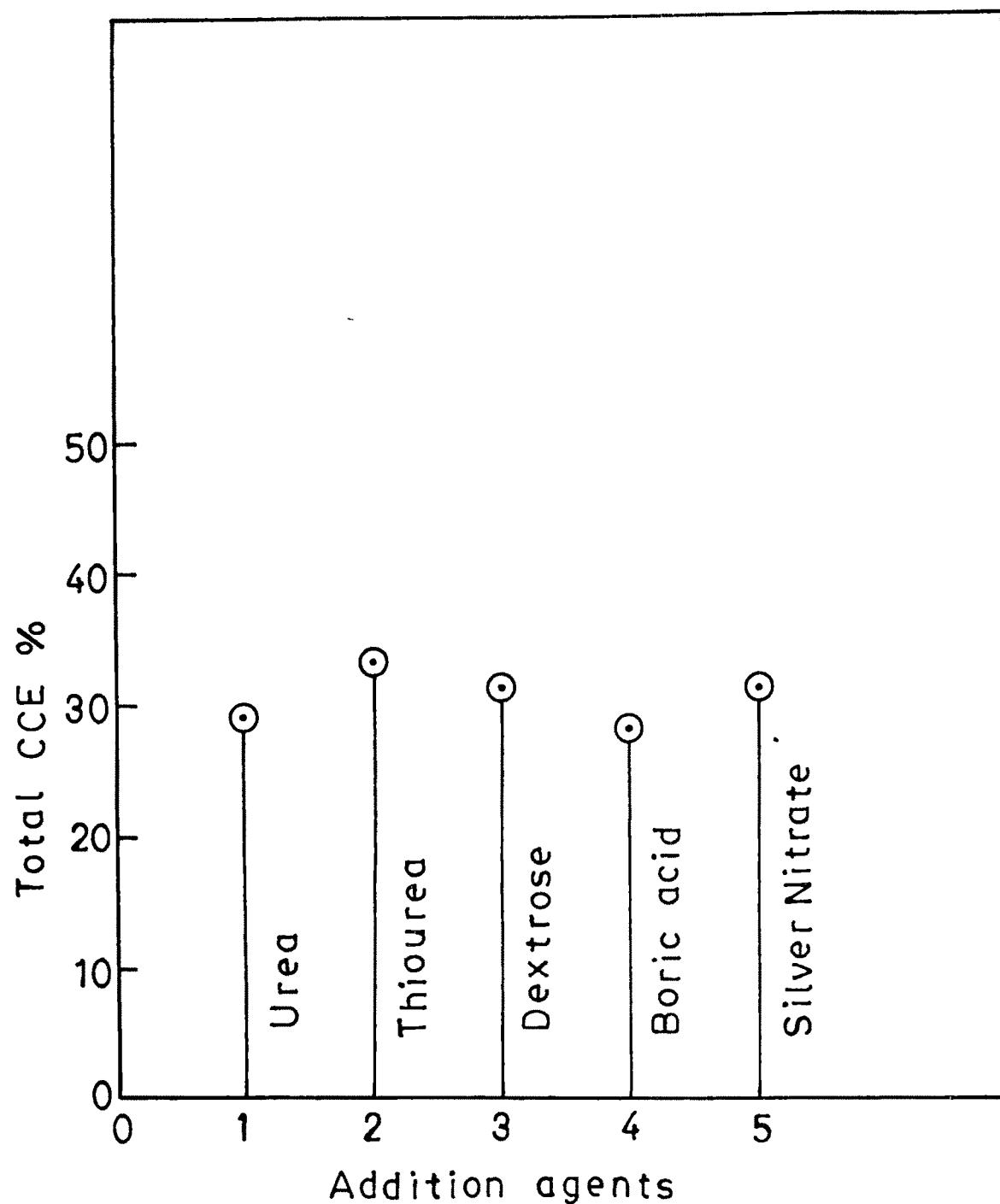
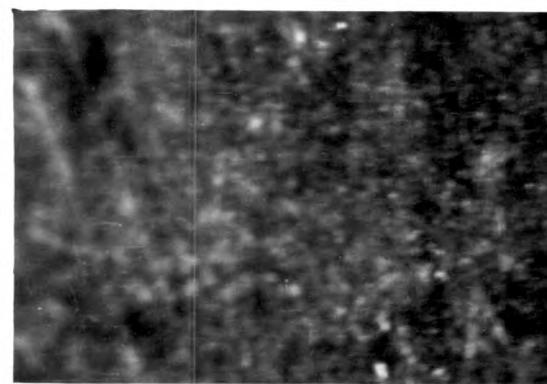


Fig. 25 – Effect of addition agents on the total CCE % of Nickel-Chromium alloy deposit .

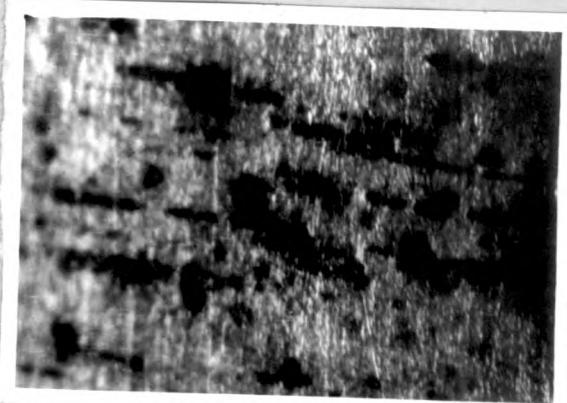
SUMMARYNICKEL-CHROMIUM SYSTEM (OPTIMUM CONDITIONS).

Table 25a: The influence of the Physico-chemical factors upon the nature and magnitude of the Ni-Cr alloy deposit has been shown in the previous Table Nos. 17 to 25 and graphically in Figs. 17-25. The ranges over which parameters were studied and optimum conditions arrived at by experiments are summarised below.

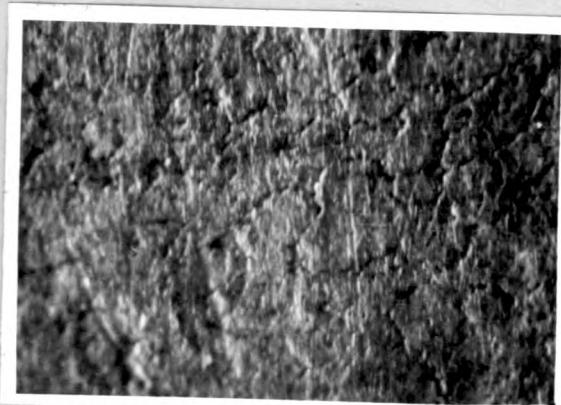
| Parameters studied and range | Optimum condition |
|---|-------------------------------------|
| 1) Composition of the bath | - |
| a) Concentration of Nickel sulphate 5-35 gms per 100 ml. of the solution. | 25 gms per 100 ml. of the solution. |
| b) Concentration of potassium chromic sulphate - 5-35 gms per 100 ml. of the solution. | 20 gms per 100 ml. of the solution. |
| c) Concentration of potassium thiocyanate 2-10 gms per 100 ml. of the solution. | 6 gms per 100 ml. of the solution. |
| d) Glycine 0-3 gms per 100 ml. of the solution. | 4 gms per 100 ml. of the solution. |
| 2) Current density. 0.5 - 4.00 amps. per Sq. dm. | 2.5 amps per sq. dm. |
| 3) Temperature 15°-55° C. | 35° C. |
| 4) Duration of Electrolysis 5-30 minutes | 20 minutes. |
| 5) Electrode distance 1-5 cms. | 2 cms. |
| 6) Silver Nitrate was used as an addition agent which remarkably improves the brightness and surface adhesency of the deposits. | |



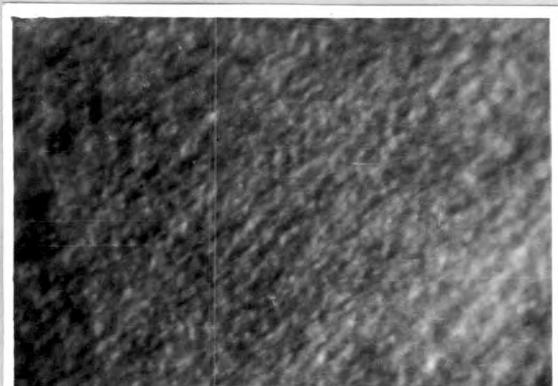
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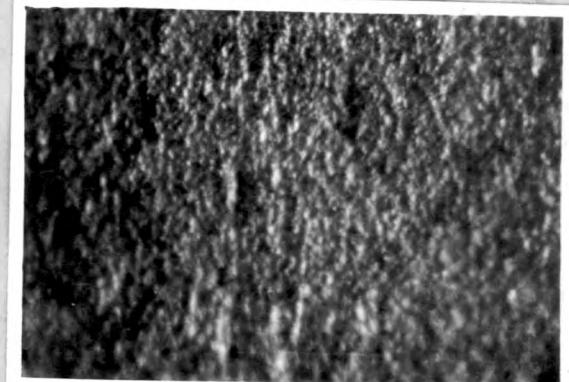
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13



14



15

cf. plate 15 (Nickel-chromium)

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4.5 Results and discussion (Table 17-25, Fig-17-25) Nickel-Chromium alloy:

The effect of different variables on the composition of the deposit, cathode current efficiency (CCE) and the nature of the deposits is described below :

Electrolyte Concentration :

1) Effect of Nickel sulphate concentration (Cf Table-17 Fig-17) :

Nickel sulphate concentration was varied from 5 gms. to 35 gms per 100 ml. of the solution. When the concentration of Nickel in the bath was increased, its content in the deposits also increased to some extent. Increase of electrolytic concentration furnishes more metallic ions and consequently increases the rate of nuclei formation and reduces the evolution of hydrogen at the cathode. This results in a uniform, fine grained and smooth deposit with greater efficiency. Higher nickel content in the bath produced dull white, unsatisfactory deposit. Similarly at low concentration of the nickel, the deposits obtained were nonadherent. Chromium content in the deposit decreased with increase in the concentration of nickel sulphate. CCE of nickel increased from 25 % to 30 % while that for chromium decreased proportionately. The optimum condition for nickel sulphate concentration was 25 gms per 100 ml, when the deposits obtained were adherent and uniform.

2) Effect of potassium chromic sulphate concentration (Cf Table -10, Fig - 10) :

The concentration of potassium chromic sulphate was changed

from 5 gms. to 33 gms. per 100 ml. of the solution. The chromium content in the alloy deposit was increased from 24 % to 31 %, while decrease in the chromium content was followed by a con-siderable increase in the efficiency upto 15 gms. of potassium chromate salt upto which the efficiency practically remained constant. The nickel content in the alloy deposit as well as the Cr-Ni in general, decreased with increase in the concentration of potassium chromic sulphate. The deposits obtained at lower as well higher concentrations of potassium chromic sulphate, were nonadherent and black. The optimum condition selected was 27 gms per 100 ml. of potassium chromic sulphate.

3) Effect of concentration of potassium thiocyanate (See Table 19, Fig. 19 & 20)

Potassium thiocyanate mainly acts as the solvent. Its concentration in the bath was varied from 2 gms. to 10 gms. per 100 ml. of the solution. For low concentration range, the deposits obtained were nonadherent. The quality of the deposit improved as there is increase in the concentration. However at high concentrations dull deposits were obtained.

4) Effect of concentration of Glycine (See Table 20, Fig. 20)

Glycine has a marked effect on the nature of the deposit and especially on Cr-Ni. As concentration of Glycine was increased the total Cr-Ni was also increased. Hence the effect of Glycine was studied using concentrations between 0 to 8 gms. per 100 ml.

of the solution. Partly shiny, uniform and satisfactory deposits were obtained at 6 A.M. per 100 ml. The deposits become dull when the concentration was further increased. The metal content as well as CCT increased with increase in the concentration of glycine. Thus, the presence of glycine improved the condition of bath as well as the CCT.

2) Effect of current density (At T = 20°C, pH = 2.1) :

According to current density normally used to improve the preparation of the best noble metal in the alloy capsule. Some addition agents may reduce this precipitation by having more effect on the precipitation behavior of one metal than on the other. The extent of the change is normally greater in simple salt solutions than in complex solutions, and greatest when the precipitating molecule are in complex ions with a common ligand thus when the nature of the complexes are different.

Using a bath of constant composition, current densities varying from 0.2 to 1.0 amp per sq. cm were selected. In the range of 0.2 to 0.4 amp per sq. cm. the same condition to the former value of current density (0.2 amp per sq. cm.) the deposits were irregular and 10% less with no change in current density upto 0.6 amp per sq. cm. more shielding voltage and adherent deposits were obtained. Above this current density, the respective current value (not shielded rotating anode, at highest Gd₂O₃ concentration 20%) due apparently to the edge, being partially to the decrease in local ion concentration near the cathode and evolution of hydrogen. The scaling effect was also observed at high I.A. (0.6 amp, pH 2.1) to

general the weight of deposit and total CEC increased with increase in current density.

c) Effect of Temperature (Cf Table - 22, Fig - 22) :

Increase in temperature usually increases the proportion of the more noble metal in the deposit. However, the effect is complicated, since the temperature change may also alter the degree of dissociation of complexes and have various effects on polarization factors. The temperature range studied was 15 - 55°C under optimum conditions of bath composition and C.R. It was seen that, the quality of deposit improved on raising the temperature to 35°C and then decreased with further rise of temperature. Increase of temperature on one hand favours diffusion and tends to produce a fine grained uniform deposit, but on the other it increases the rate of crystal growth, decreases the hydrogen overvoltage, favouring evolution of H₂ gas and causes the precipitation of basic salts, resulting in a coarse, poorly adherent and dark deposit. At moderate temperatures the influence of the former factor is predominating while at higher temperatures latter ones are increasingly operative. Chromium content in the alloy deposit and CEC increased slightly, while the Nickel content in the alloy deposit and its CEC decreased proportionally with an increase in the temperature. This is somewhat unusual because an increase ⁱⁿ the temperature, usually tends to increase the proportion of more noble metal in the alloy plate. However, the variation being very small the point need not be stressed further.

7) Effect of duration of electrolysis (see table -23, Fig-23) :

At the optimum concentrations, current density and temperature, the duration of electrolysis was varied from 5 minutes to 30 minutes. The total cathode current efficiency of the deposit was found to increase from 31 % to 41 % over the whole range of duration studied. The metal contents both nickel and chromium increased in general with increase in the duration of electrolysis. The nature of the deposits, were found unaffected for different periods, except at 5 minutes nonadherent deposits were obtained.

8) Effect of distance between electrodes (see Table -24, Fig-24) :

The distance between cathode and anode was changed between 1-5 cm. It was noticed that the character of the deposit was not affected to any appreciable extent, either qualitatively or quantitatively, excepting that the cathode current efficiency tends to decrease with increase in the distance between cathode and anode.

9) Effect of addition agents (see Table 25, Fig- 25) :

The addition agents listed in Table 25 were introduced singly to the bath under the optimum conditions and the effect was studied. In presence of gum, chlorine and dextrose the quality of the deposit was considerably improved and bright white, adherent deposits were obtained. The deposits obtained in presence of silver nitrate was lustrous, bright, and uniform. The silver was not detected during the quantitative analysis in

the deposit. The composition and A.R. remained more or less the same for all observations.

It is well known that even small quantities of certain substances added to a depositing solution markedly influence the structure of the resulting deposit. These are called as addition agents. Most of them are colloidal in nature and they form disperse systems with the electrolyte. They produce marked change in the character and structure of the deposit. Small quantities of the colloidal addition agents may cause the metal to collect as very small crystals and produce a smooth, uniform and adherent deposit. Also, current density on the cathode surface is never perfectly uniform. There may be a few points on the surface which being nearer to the cathode receive more of the current. The crystal growth at these points will be faster. But when colloidal particles are present, due to higher current density, they preferentially collect at these points constituting a non conducting layer around them, until the general level of the metal builds upto them, thus producing a smoother deposit.

At this background, the influence of addition agents listed in Table - 25 could be explained in relation to observations stated earlier.

4.5.2 The Role of Silver as an addition agent in alloy-depositions

Crustous, white shining deposit of silver can be obtained on a base metal from well known silver baths. Silver or any noble metal can easily be plated out from a plating solution in preference to any other metal preceding the same in HS series, due to hydrogen-over voltage and uniform, stirring of the plating solution (polarization effects being minimised). Co-deposition of the metals can be achieved. In a solution containing sufficient amounts of a noble metal and another base metal, the latter can be co-deposited with silver, / metal contents of the two metals in the alloy ^{depend on} their relative proportions in the plating solutions, differences in reversible potentials and overvoltages of the depositing ions (Cf equation - 4) govern the Codeposition.

However, in presence of silver added to the plating solution, in traces, there appears to be no possibility of silver depositing simultaneously with nickel and chromium which are in much larger quantities in the bath solution as denoted by the equation - 4. This is confirmed by analysing the deposit in which silver was not detected. However, the remarkable improvement in the nature of the deposit suggests, the possibility of silver acting as an addition agent in the alloy

deposition. The experimental conditions would tend to exclude any silver to be detected in the alloy deposit. However, it can be argued that silver entering into the Ni-Cr alloy structure by substitution, leading to a solid solution could not be up to the limit of detection by our analytical methods. It is this silver present in traces in the alloy deposit, which renders its shining properties to the alloy, giving it an appearance of silver deposit.

Alternatively, silver added in traces may get transformed into colloidal silver hydroxide acting as an addition agent which may cause the other two metals to collect as very small crystals and produce the observed effects, or it may be that the colloidal silver hydroxide constitutes a non-conducting layer around the points of higher current density at the cathode, thus producing a silvery shining deposit of the alloy.

The resulting alloy has much superior qualities of noble metals as compared to the stainless steel coatings obtained by Rama Shriram (79) for nickel, chromium and iron alloy system.

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